

1 **Title: Detection, fate and inactivation of pathogenic Norovirus employing**
2 **settlement and UV treatment in wastewater treatment facilities.**

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17 **Running title:** *Detection, fate and inactivation of pathogenic Norovirus employing settlement and UV*
18 *treatment in wastewater treatment facilities.*

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21 human health.

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26 **Abstract**

27 It is accepted that discharged wastewaters can be a significant source of pathogenic viruses in
28 receiving water bodies contributing to pollution and may in turn enter the human food chain
29 and pose a risk to human health, thus norovirus (NoV) is often a predominant cause of
30 gastroenteritis globally. Working with NoV poses particular challenges as it cannot be readily
31 identified and detection by molecular methods does not assess infectivity. It has been
32 proposed that the infectivity of NoV may be modelled through the use of an alternative virus;
33 F-specific RNA (FRNA) bacteriophages; GA genotype and other FRNA bacteriophages have
34 been used as a surrogate in studies of NoV inactivation.

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36 This study investigated the efficiency of novel pulsed ultraviolet irradiation and low pressure
37 ultraviolet irradiation as a potential pathogen inactivation system for NoV and FRNA
38 bacteriophage (GA) in secondary treated wastewaters. The role of UV dose and the impact of
39 suspended solids concentration on removal efficiency were also examined. The study also
40 investigated the role of settlement processes in wastewater treatment plants in removing
41 NoV. While NoV inactivation could not be determined it was found that at a maximum UV
42 dose of 6.9 J/cm^2 (6900 mJ/cm^2) an average 2.4 log removal of FRNA bacteriophage (GA)
43 was observed; indicating the potential need for high UV doses to remove NoV if FRNA
44 bacteriophage prove a suitable indicator for NoV. The study found that increasing
45 concentrations of suspended solids impacted on PUV efficiency however, it appears the
46 extent of the impact may be site specific. Furthermore, the study found that settlement
47 processes can play a significant role in the removal of FRNA bacteriophage, thus potentially
48 NoV.

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60 **1.0 Introduction**

61 The release of treated and untreated effluent to water-bodies is a global occurrence and can
62 be a significant source of pathogenic viruses. Norovirus (NoV) is one such pathogenic virus,
63 which has garnered significant attention particularly in the public health sector and shellfish
64 industry. Noroviruses (NoVs) are small single stranded RNA viruses that are members of the
65 Caliciviridae family. The species is subdivided into five separate genotypes, Genogroups I
66 (GI), II (GII), III (GIII), IV (GIV) and V (GV) (da Silva *et al.*, 2007). Typically GI and GII
67 predominate (da Silvia *et al.*, 2007; Scallan *et al.*, 2011; Ahmed *et al.*, 2014). As diagnostic
68 methods for NoV infection have improved there has been growing recognition of its
69 importance in response to growing incidence of NoV infection. NoV is now accepted as the
70 most common aetiological agent of sporadic acute gastroenteritis in many communities,
71 posing a particular risk to young, elderly and immune-compromised individuals (Nordgren *et*
72 *al.*, 2009; CDC, 2012). NoV also accounts for a high proportion of community and hospital
73 outbreaks of acute self-limiting gastroenteritis infection (Lopeman *et al.*, 2004; da Silvia *et*
74 *al.*, 2007; Nordgren *et al.*, 2009; Ahmed *et al.*, 2014). Direct person to person transmission of
75 NoV and transmission in contaminated indoor environments (hospitals, long term care
76 facilities and cruise ships) have been established as important factors in the spread of
77 infection.

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79 Food and waterborne transmissions however are also of concern and in this context
80 discharges of human effluent containing large numbers of virus particles (10^{11} viruses/gram
81 of faeces) is a concern (Atmar *et al.*, 2008). Inadequate wastewater treatment can result in the
82 persistence of viruses and microorganisms leading to environmental pollution, economic
83 impacts and risk to human health (da Silva *et al.*, 2007; Cheng *et al.*, 2012). To date most
84 technology development and regulation related to wastewater treatment has focused on
85 organic carbon, suspended solids (SS), nutrient and general microbial removal from
86 discharged wastewaters. While wastewater treatment plants (WWTPs) can contribute to virus
87 removal it is widely accepted that specifically designed process are required to fully remove
88 or inactivate viruses (Ottoson *et al.*, 2006; Nordgren *et al.*, 2009; EPA, 2016). However,
89 molecular methods for the detection of NoV do not reliably differentiate between active and
90 inactivated viruses which are a major limitation in the evaluation of the effectiveness of
91 methods such as ultraviolet irradiation (UV) which does not remove the virus but rather
92 inactivates it.

93 There is a need for robust RNA based identification tools to critically evaluate, not just the
94 genomic viral load, but distinguish between non-infectious and infectious NoV (Gibson *et al.*,
95 2012; Vinjé, 2015). Advances in molecular applications have permitted increased
96 investigation into infection rates associated with the specific NoV genogroups and their
97 pattern of distribution (Franck *et al.*, 2015). However, the sensitivity and quantitative ability
98 of RT-qPCR is overshadowed by its inability to distinguish between infectious and non-
99 infectious viral loads.

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101 Surrogates, such as those from the Caliciviridae family have been studied as possible
102 indicators to determine the level of NoV viral contamination. It is widely agreed that their use
103 may allow adequate assessment of the environmental persistence of NoV (Dore & Lees,
104 1995; Flannery *et al.*, 2012). Surrogates suggested for NoV detection include the murine
105 calicivirus, feline calicivirus, tulane virus and the male-specific or F-specific RNA (FRNA)
106 bacteriophages (Dore *et al.*, 2000; Karst *et al.*, 2003; Cannon *et al.*, 2006; Hirneisen &
107 Kniel, 2013; Kniel, 2013). The FRNA bacteriophage (GA) is a human-specific phage strain
108 that lies within the Levivirus genogroup II. It is morphologically and physio-chemically
109 similar to NoV and it may also be cultivated i.e. infectivity can be determined, thus it has
110 been suggested as a robust choice of NoV surrogate and was used in this study.

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112 Current European regulations do not require monitoring of viral loads in treated wastewater
113 which can be an intense source of pathogenic viruses. WWTPs generally comprise a number
114 of stages including primary treatment, (generally removal of larger solid matter), secondary
115 treatment, (generally biological treatment of wastewater) and tertiary treatment (further
116 treatment of wastewater or removal of targeted pollutants). It is widely accepted that primary
117 and secondary wastewater treatment systems do not fully remove viruses or FRNA
118 bacteriophages (Nordgren *et al.*, 2009; Ottoson *et al.*, 2006). Tertiary treatment such as
119 pathogen removal is increasingly crucial in order to comply with strict regulations, such as
120 those that may necessitated by implementation of the Water Framework Directive (WFD -
121 2000/60/EC), Surface Waters Regulations (S.I. No. 272 of 2009) and the European
122 Community Shellfish Waters Directive (2006/113/EC) or to enable opportunities for
123 wastewater reuse. Ultraviolet (UV) disinfection is frequently preferred in the wastewater
124 treatment sector (where pathogen removal technologies are deployed) as it limits production
125 of harmful by products that require further processing and is a cost-effective option both
126 terms of capital costs and running costs (Moghadam & Dore, 2012; EPA, 2016). UV

127 processes are divided into three main categories (1) low pressure/low intensity lamps (2) low
128 pressure/ high intensity lamps (3) medium pressure/high intensity lamps. These systems vary
129 with respect to operating pressure and output level and it is low and medium pressures that
130 are employed in the treatment of wastewater (Whitby & Scheible, 2004; Leong *et al.* 2008).
131 A further consideration is the upstream performance of a WWTP which can have significant
132 impacts on the efficacy of downstream UV technologies. While turbidity and suspended
133 solids can have a negative effect on UV disinfection by decreasing transmissivity (the
134 transmission of UV light through the water body) these factors are not routinely considered
135 when monitoring UV performance.

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137 Low pressure (LP) UV disinfection results in photochemical damage to the DNA or RNA of
138 the microorganism thus inhibiting reproduction leading to eventual cell death. It is worth
139 noting however, that photoreactivation or ‘dark repair’ can occur post UV disinfection in
140 wastewater, albeit mainly in bacteria strains (Guo *et al.*, 2011; Goosen & Moolenaar, 2008).
141 Recently pulsed UV (PUV) light technology has been investigated as an alternative to
142 existing technologies. PUV offers the capability to better control discharge energy and UV
143 dosage (J/cm^2 / mJ/cm^2) by varying the operating voltage of the unit or the frequency of
144 discharges (Garvey *et al.*, 2010; 2015).

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146 The objectives of this study were to examine the effectiveness of using conventional low
147 pressure UV irradiation and novel high-intensity pulsed UV disinfection in removing NoVs
148 (via a FRNA bacteriophage (GA) surrogate) from secondary treated wastewater. The study
149 also focused on the role of settlement processes in removing NoV within WWTPs and the
150 impact of SS on UV system performance.

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152 **2.0 Materials and Methods**

153 **2.1 Source of wastewater**

154 Samples for this study were taken from three municipal activated sludge WWTPs (WWTP 1,
155 2 and 3), whereby WWTP 1 was used for the majority of the study and the remaining two
156 WWTP were used to ascertain the effect of SS on disinfection performance. WWTP 1
157 comprised primary and secondary treatment systems with phosphorus removal via ferric
158 sulphate addition and tertiary treatment by sand filtration. WWTPs 2 and 3 comprised
159 primary and secondary treatment systems with WWTP 2 also featuring a LP UV system. The
160 WWTPs ranged in size from 21,000 population equivalent (WWTP 1) to 250 (WWTP 2) and

161 3,500 (WWTP 3). All received municipal wastewater from combined storm and municipal
162 sewers.

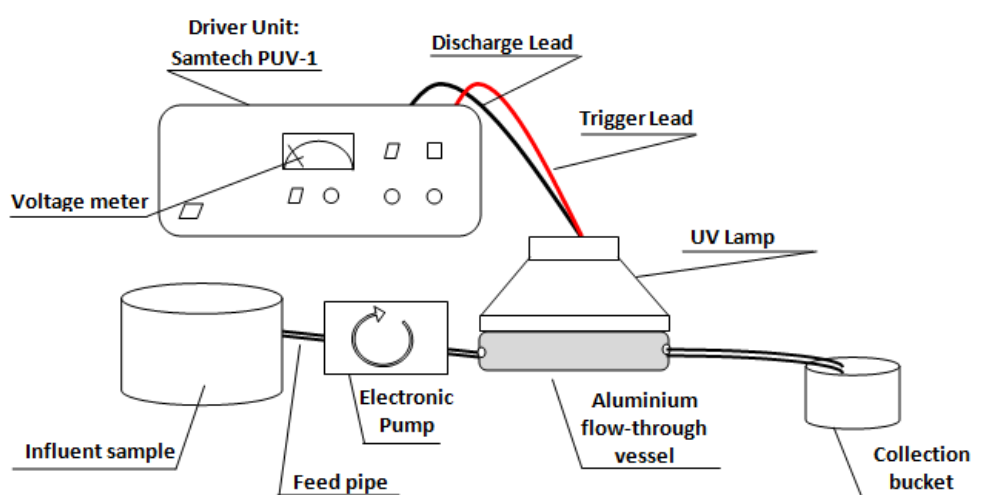
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164 2.2 Pulsed UV irradiation

165 Secondary effluent was sampled at an effluent sampling point in WWTP 1. Samples were
166 transported to the laboratory and were stored at constant temperature (10 °C) prior to
167 processing. A bench-scale pulsed power source (PUV – 1, Samtech Ltd., Glasgow) was used
168 to power a low pressure (60 kPa) xenon-filled flashlamp (Heraeus Noblelight XAP type
169 NL4006 series constructed from a clear UV transparent quartz tube) which produced a high
170 intensity beam of polychromatic pulsed light. The lamp was placed 10 cm above a sterilised
171 aluminium flow- through vessel which pumped secondary effluent through the vessel at the
172 desired flow rate (Figure 1). The system when operating at 900 V and 5.6 pulses per second
173 (PPS) - gave a maximum dose of 6.9 J/cm² (6900 mJ/cm²) at a hydraulic residence time
174 (HRT) of 120 s. The PUV system allowed for the input voltage and the pulse rate to be varied
175 between 300 and 900 V and 0.1 and 10 PPS.

176

177 As a control, wastewater batches (secondary effluent and distilled water; 7 L) were “spiked”
178 with known quantities of NoVs (genogroup I (GI) and genogroup II (GII)) and FRNA
179 bacteriophage (GA) to accurately measure log reduction. These were processed using the
180 bench-scale novel PUV system in the same conditions as used on the effluent samples and the
181 results compared against the “spiked” concentrations.



182

183 **Figure 1** Schematic of the bench-scale PUV experimental set-up.

184

185 To ascertain the effect various wastewater parameters (suspended solids, total organic carbon
186 and total inorganic carbon) had on PUV viral inactivation in secondary effluent four
187 experimental trials (Trials 1 – 4) were carried out on separate days (where the number of runs
188 carried out on each day varied between 1 (trial 1) and 3 (trials 2, 3 and 4), examining FRNA
189 bacteriophage (GA; infectivity assay) inactivation/removal. The effect of SS on PUV
190 efficiency was investigated over 10 trials in total in terms of GA bacteriophage removal.
191 During Trials 2, 3, and 4 secondary effluent (7 L) was spiked with a known concentration of
192 mixed liquor suspended solids (MLSS) and seeded with a known concentration of FRNA
193 bacteriophage (GA). Samples were collected pre and post treatment. The flow through the
194 PUV system was controlled to give hydraulic residence times of 60 s HRT and a UV dosage
195 of 3.4 J/cm^2 (3400 mJ/cm^2) and 120 s HRT resulting in a UV dosage of 6.9 J/cm^2 (6900 mJ/cm^2).
196 cm^2).

197

198 Batches (25 L) of secondary treated wastewater samples were collected from three separate
199 WWTPs – 1, 2 and 3. Five litres from each batch was then seeded with a known quantity of
200 GA bacteriophage and pumped through the PUV system at two HRTs; 60 s HRT (3.4 J/cm^2 ;
201 3400 mJ/cm^2) and 120 s HRT (6.9 J/cm^2 ; 6900 mJ/cm^2). Influent and effluent samples to
202 and from the PUV system were collected and analysed in each case. For comparison, separate
203 5 L samples from each batch of the aforementioned 25 L samples were filtered using 0.1 - 0.2
204 μm filter removing all SS. The same procedure for the unfiltered samples was then applied to
205 the filtered samples and the results were compared to the unfiltered samples.

206 **2.3 Comparison between PUV and low pressure UV systems**

207 WWTP 2 comprised a LP UV treatment system (AquaPRO, UV12GPM-HTM) which treated
208 wastewater from a secondary treatment process with a clarifier. During this study grab
209 samples (1 L) were collected at both the influent and effluent points of the LP UV system to
210 investigate pathogen removal. In order to draw a direct comparison, 6 x 5 L grab samples of
211 the wastewater influent to the LP UV system were collected for processing via the bench-
212 scale PUV system. These samples were taken concurrently with the aforementioned 1 L
213 samples.

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215 The grab samples for the PUV system were immediately stored in a refrigerator at $4 \text{ }^\circ\text{C}$,
216 transported to the laboratory and were processed via the bench-scale PUV system within 24
217 hours. The operating details of the LP UV and PUV systems are outlined in Table 1.

218 Following this, three categories of pathogen inactivation/removal were examined via LP UV
 219 and PUV; *E. coli*, total coliforms and FRNA bacteriophage (GA). The comparison between
 220 the LP UV and PUV systems were carried out in duplicate on three consecutive days. The LP
 221 UV system was operated at three flow rates (resulting in three hydraulic residence times
 222 (HRT's); 0.23 m³/hr, 0.52 m³/hr and 0.85 m³/hr. These resulted in UV dosage rates of 0.117
 223 J/cm² (117 mJ/cm²), 0.0516 J/cm² (51.6 mJ/cm²) and 0.0316 J/cm² (31.6 mJ/cm²),
 224 respectively.

225 **Table 1.** Operational detail of LP UV and PUV .

(Day)	LP UV			PUV
(1)				
Flow Rate (m ³ /hr)	0.23	0.52	0.85	0.04
UV Dose - J/cm ² (mJ/cm ²)	0.117 (117.0)	0.0516 (51.6)	0.0316 (31.6)	3.4 (3447.8)
(2)				
Flow Rate (m ³ /hr)	0.220	0.529	0.818	0.04
UV Dose - J/cm ² (mJ/cm ²)	0.122 (122)	0.050 (50.7)	0.0328 (32.8)	3.4478 (3447.8)
(3)				
Flow Rate (m ³ /hr)	0.209	0.526	0.810	0.04
UV Dose - J/cm ² (mJ/cm ²)	0.1284 (128.4)	0.051 (51)	0.0331 (33.1)	3.4478 (3447.8)

226

227 **2.4 Fate of both NoV and FRNA bacteriophage (GA strain) in wastewater treatment**
 228 **plants**

229 To ascertain the fate of NoV and FRNA bacteriophage through WWTP1, 2 L batch samples
 230 of wastewater were collected from five sampling points at the WWTP; raw influent (R),
 231 primary clarifier (PT), the activated sludge reactors and the secondary clarifier (ST) on two
 232 separate sampling days. The activated sludge reactor was divided into two samples; the
 233 sample as taken from the reactor (Sample A) and a sample (Sample AS) representing the
 234 clarified portion was collected following 24 hours of settlement in a graduated cylinder. In all
 235 cases samples were transported at 4 °C before immediate processing (detailed below).

236

237 **2.4 Measurement of wastewater characteristics**

238 Suspended solids (SS) were measured in accordance with standard methods (APHA, 2005).
239 Total organic carbon (TOC) and total inorganic carbon (TIC) were measured using the
240 Biotector TOC, TN, TP Analyser (Biotector Analytical System Ltd., Cork, Ireland) in
241 accordance with standard methods. Results were expressed in mg/L. Wastewater samples
242 were tested for iron and manganese levels by Environmental Laboratory Services (ELS) Ltd
243 Acorn Business Campus, Mahon Industrial Park, Blackrock, Cork, Ireland. Five litre batch
244 samples were collected; 2 L of each sample was filtered through a 0.1 µm membrane cassette
245 (Pall's Omega™ polyethersulfone [PES]; Fitzhenry *et al.*, 2014). One x 75 mL sample of
246 both unfiltered and filtered effluent from each site was held in a storage vial at the correct pH
247 at 4 °C. All samples were collected after two days and couriered to ELS for metals analysis.
248 The LOQ of the tests were 5 µg/L and 1 µg/L for iron and manganese respectively.

249

250 **2.4 Extraction procedure for NoV and FRNA bacteriophage (GA) analysis**

251 Harvested samples were concentrated from 40 mL to 500 µL using a virus adsorption-elution
252 method previously described in Fitzhenry *et al.* (2014) and Flannery *et al.* (2013). The
253 resulting 500 µL underwent RNA extraction employing NucliSENS miniMAG extraction
254 platform and the corresponding NucliSENS magnetic extraction reagents. Samples were then
255 stored at -80 °C prior to further processing. The use of a non-related virus (Mengo virus) was
256 also employed as an 'internal process control' (IPC) to determine the extraction efficiency
257 (Costafreda *et al.*, 2006). A negative RNA extraction control, molecular grade water (Bioline)
258 was additionally processed alongside the samples.

259

260 **2.5 Microbiological analysis**

261 Samples were processed using both molecular and cultivation-dependent analyses. NoV GI
262 and GII analysis was carried out via molecular methods only while FRNA bacteriophage
263 (GA) was processed by both molecular analysis and microbiological culture analysis.

264

265 **2.5.1 Microbiological culture analysis**

266 *FRNA bacteriophage (GA)*

267 A standardised plaque assay coupled with an in-situ hybridisation assay was employed to
268 determine infectious FRNA bacteriophage (GA) and to distinguish between genotypes
269 (Sundram *et al.*, 2006). *Salmonella enterica* serovar Typhimurium WG49 was used as a host
270 strain in order to enumerate the FRNA bacteriophage (GA) using a double - layer overlay

271 plaque assay as previously outlined in Flannery *et al.* (2013). Briefly, 1 mL of appropriately
272 diluted sample was added to 1 mL of host culture (*Salmonella Typhimurium* WG49) and 2.5
273 mL of molten tryptone – yeast glucose agar and held at 45 °C. This mix was then poured onto
274 hardened tryptone – yeast glucose agar plates and left to solidify before being transferred to a
275 37 °C incubator for 18 ± 2 hours inverted. Once the incubation period had passed, the plates
276 were removed and characteristic plaques were counted by visual inspection, where each
277 plaque was assumed to originate from one GA bacteriophage. The results were expressed as
278 plaque forming unit (pfu)/mL. The Limit Of Detection (LOD) for this test was 1 pfu/mL.
279 Additionally an internal positive culture control was run alongside the environmental samples
280 to ensure the assay was performed to capacity.

281

282 *Escherichia coli* (*E. coli*) enumeration in wastewater

283 Total coliforms were enumerated using the Quanti – Tray Colisure test, IDEXX based on the
284 most probable number method (MPN). The standardised five-tube, three-dilution MPN; ISO-
285 TS 16649) was used to assess the presence/reduction of *E. coli* in UV influent and UV treated
286 effluent wastewater samples. Appropriate log₁₀ dilutions of samples were inoculated into 10
287 mL volumes of minerals modified glutamate broth (MMGB; CM0607, Oxoid) and were
288 incubated at 37 °C for 24 ± 2 h. The presence of *E. coli* was subsequently confirmed by sub-
289 culturing tubes indicating acid production onto Tryptone Bile Xglucuronide (TBX) agar
290 (CM0945, Oxoid) at 44 °C for 22 ± 2 h. The limit of detection (LOD) of the assay was 20 *E.*
291 *coli*/100 mL.

292

293 **2.5.2 Microbiological molecular analysis**

294 A one step Reverse Transcriptase Quantative Polymerase Chain Reaction (RT-qPCR) was
295 employed to enumerate NoV GI, NoV GII and FRNA bacteriophage (GA). During this
296 process, extracted RNA was reverse transcribed into its complementary double stranded
297 plasmid DNA (dsDNA) sequence and was quantified. Standard curves for quantification of
298 the three targets (NoV GI, NoV GII and FRNA bacteriophage (GA) were constructed using
299 dsDNA corresponding to each virus and primer/probe sets and thermal cycling protocol, as
300 outlined in detail in Flannery *et al.* (2012; 2013; Table 2). Briefly to create a standard curve, a
301 10-fold serial dilution series, ranging from 10⁵ down to 10¹ copies (of each target) μL⁻¹ was
302 generated and analyzed in duplicate by real-time PCR using Applied Biosystems AB7500
303 qPCR instrument with the corresponding primer/probe sets (Table 2). Five microlitres of
304 sample RNA were added in duplicate to the wells of a 96 – well optical reaction plate with 20

305 μ L one-step mastermix (Invitrogen). NoV GI, GII and GA FRNA bacteriophage were
306 quantified by comparing the Cq values to the appropriate standard curves in copies per mL,
307 and then adjusted to reflect the volume of RNA analysed (expressed as genome copies g_1
308 HP or genome copies 100 mL_1 wastewater). The Limit Of Quantification (LOQ) for this
309 test was 125 copies/100 mL and the Limit Of Detection (LOD) was 25 copies/100mL. For
310 extraction efficiency (determined using the IPC; Mengo virus; Table 2) previously described
311 forward (Mengo209) and reverse (Mengo110) primers and probe (Mengo147) were used
312 (Pinto *et al.*, 2009) and was performed as outlined in detail in Flannery *et al.* (2012). The Cq
313 value of the sample was compared to a standard curve obtained by preparing log dilutions
314 from the same batch of Mengo virus as was used to spike samples for analysis. This was
315 expressed as percentage extraction efficiency and samples with an extraction efficiency of
316 less than 1 % were not accepted.

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Table 2: The suite of RT-qPCR primers and probes utilized in this study.

Target	Probe	Primer	Sequence (5' to 3')	Reference
NoV GI	NVGG1p	Forward- QNIF4	VIC-TGGACAGGAGAYCGCRATCT- TAMRA CGCTGGATGCGNT TCCAT	Svraka <i>et al.</i> , 2007
		Reverse- NV1LCR	CCTTAGACGCCATCATCATTTAC	
NoV GII	QNIFS	Forward- QNIF2	FAM-AGCACGTGGGAGGGCGATCG- TAMRA ATGTTTCAGRTGGATGAGRTTCTCWGA	Loisy <i>et al.</i> , 2005
		Reverse- COG2R	TCGACGCCATCTTCATTCACA	
FRNA Bacteriophage (GA)	Genogroup I- Probe	Forward- Genogroup I-	CAWGGTAGCGTCTCGCTAAAGACATT GTCCTGCTCRACTTCCTGT	Wolf <i>et al.</i> , 2008
		Reverse - Genogroup I	CGGCTACCTACAGCGATAG	
Mengo virus	Mengo147	Forward- Mengo209	ATCACATTACTGGCCGAAGC GAAGTAACATATAGACAGACGCA CAC	Costafreda <i>et al.</i> , 2006
		Reverse- Mengo110	GCGGGTCCTGCCGAAAGT	
				Pintó <i>et al.</i> , 2009

341

342 2.6 Calculation of log reductions

343 Log reductions of NoV GI, NoV GII and FRNA bacteriophage (GA) were calculated by
344 determining the absolute of each target before and after treatment with bench-scale PUV and
345 On-site LP UV, respectively.

346

347 2.7 Statistical analysis

348 In order to evaluate any differences between NoV GI and NoV GII concentrations in the
349 environmental samples and between concentrations of infectious and total FRNA
350 bacteriophage GA, minitab statistical software was used to carry out nonparametric tests

351 (MannWhitney Rank Sum Test) and Microsoft excel was used for correlation coefficient
352 analysis.

353

354 **3.0 Results and Discussion**

355 **3.1 Comparison of molecular and culture viral enumeration methods and potential the** 356 **use of FRNA Bacteriophage (GA) as surrogate for NoV**

357 In this study the effect of PUV disinfection on virus inactivation in wastewater was measured
358 over the HRTs of 60 (UV dose – 3.4 J/cm²; 3400 mJ/cm²) and 120 seconds (s) (UV dose –
359 6.9 J/cm²; 6900 mJ/cm²), pulsed UV intensity and at varying SS concentrations. In parallel
360 with molecular analysis targeting NoV GI and GII and GA bacteriophage via RT–qPCR,
361 FRNA bacteriophage (GA) via infectivity assay pre and post PUV treatment (n = 10) were
362 also studied as an indicator of infectivity. Results for the infectivity assay showed an average
363 2 log₁₀ mean reduction of FRNA bacteriophage (GA) at a HRT of 120 s (UV dose – 6.9
364 J/cm²; 6900 mJ/cm²) over the entire study period. The starting GA bacteriophage copy
365 concentrations (0 s) were significantly different to NoV GI and GII viral copy concentrations
366 following PUV treatment at 60 s ($p = 0.0002$) and at 120 s ($p = 0.0002$; UV dose – 6.9 J/cm²
367 (6900 mJ/cm²) at a 95% confidence interval (Figure 2). The overall copy concentrations
368 varied significantly between PUV treatment at HRT's of 60 s and 120 s (UV doses – 3.4
369 J/cm² (3400 mJ/cm²) and 6.9 J/cm² (6900 mJ/cm²), respectively, at a 95 % confidence
370 interval ($p = 0.0211$). The average reduction of FRNA bacteriophage (GA), NoV GI and NoV
371 GII as measured by RTqPCR was < 0.5 log₁₀, thus there was little or no reduction of copy
372 concentrations at the maximum UV doses applied throughout the study (6.9 J/cm² (6900
373 mJ/cm²); all stated PUV dosage rates relates to wavelengths < 300 nm; (Figure 2; Table 3).
374 NoV GI results yielded significant differences pre and post PUV treatment at 60 s ($p =$
375 0.0409) and 120 s ($p = 0.0298$) and also between PUV treatments (60s and 120s; $p = 0.0409$)
376 at 95 % confidence interval.

377

378 While the data indicates significant differences in the recorded copy concentrations pre and
379 post PUV treatment, it is not representative of the reduction of infectious virus. Therefore in
380 this incidence, RT–qPCR was not appropriate method of assessing the inactivation of NoV
381 and FRNA bacteriophage (GA) via PUV post UV treatment. This may be possibly due to the
382 fact that genomic debris resulting from UV treatment can result in false-positive PCR signals
383 (Pecson *et al.*, 2010). As viable NoV concentrations could not be assessed post PUV
384 treatment, findings in this study could not draw direct comparisons between FRNA

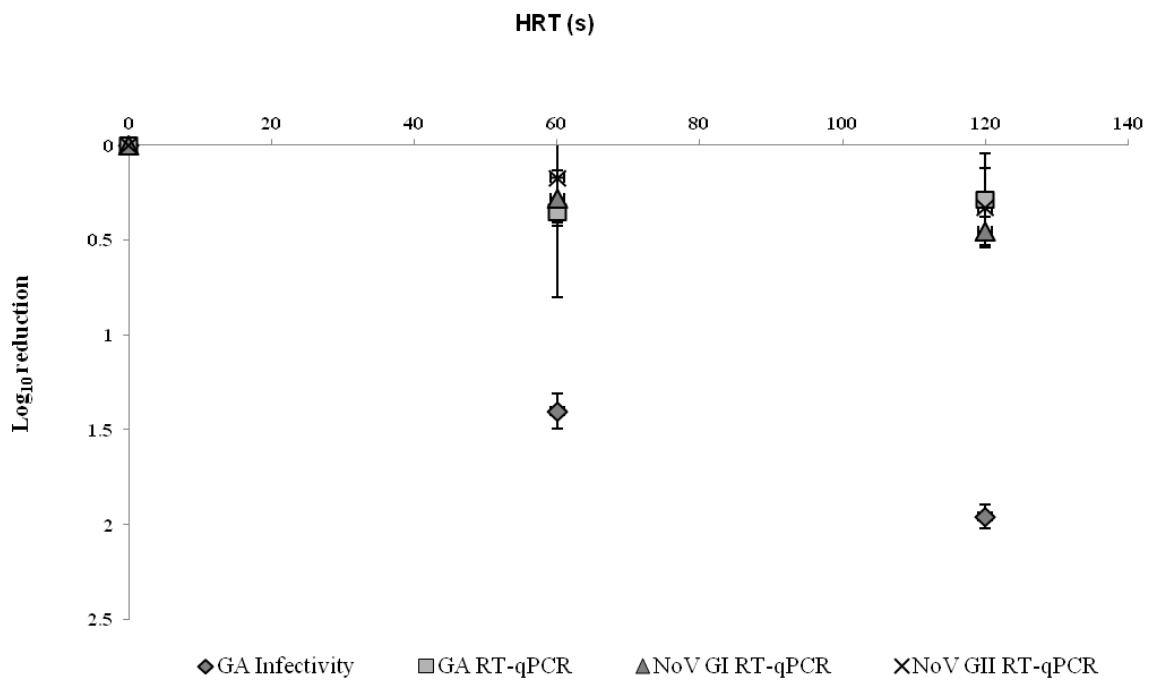
385 bacteriophage (GA) and NoV reductions. However, due to the high resistance properties of
386 FRNA bacteriophage (GA) to PUV treatment and its morphological similarities to NoV, this
387 would indicate that the use of this virus as a potential surrogate may have value and would
388 warrant further analysis based on previous studies (Doré *et al.*, 2000; Flannery *et al.*, 2012).

389

390 Similar to this study, Baert *at al.* (2008) found RT-qPCR results were unable to distinguish
391 between infections and non-infectious NoV, using murine norovirus (MNV) as a surrogate;
392 no correlation was seen when comparing an infectivity assay and RT-qPCR for the detection
393 of MNV examining virus inactivation using heat treatment. Conversely, when comparing
394 infectivity assays and RT-qPCR, Bae and Schwab (2008) determined that MNV, FRNA
395 coliphage MS2, and poliovirus (PV) all have the potential to be useful surrogates for human
396 NoVs and are the most robust choice of NoV identification. In order to efficiently distinguish
397 between infectious and non-infectious NoV, investigative focus has moved towards firstly the
398 optimisation of targeting relevant gene sequences to permit the generation of specific primer
399 and probes for infections/non-infectious identification, independent of culture based systems.
400 This in itself is extremely challenging as only one small region is adequately conserved
401 enough to construct specific genogroup oligonucleotide primers and probes (Green *et al.*,
402 2001; Katayama *et al.*, 2002; Zheng *et al.*, 2006; Vinjé, 2015).

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Figure 2. Average log₁₀ reduction of viable FRNA bacteriophage (GA; infectivity assay; n = 10) and copy number of FRNA bacteriophage (GA) and norovirus GI and GII (RT-qPCR; n = 7) post PUV treatment in wastewater. (The average initial concentration was 10⁶/100 mL).

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435 **Table 3.** Log₁₀ reduction of infective FRNA bacteriophage (GA; n = 10) as tested by the
 436 infectivity assay and copy concentrations of FRNA bacteriophage (GA) and norovirus GI and
 437 GII (n = 7) as tested by RT-qPCR post PUV treatment in wastewater (60 s HRT: UV dose –
 438 3.4 J/cm² (3400 mJ/cm²), and 120 s HRT: UV dose 6.9 J/cm² (6900 mJ/cm²); the average
 439 initial concentration was 10⁶/100 mL).

Infectivity Assay				RT-qPCR Assay			
FRNA bacteriophage (GA)		FRNA bacteriophage (GA)		NoV GI		NoV GII	
Log ₁₀ removal at HRT ± standard deviation		Log ₁₀ removal at HRT ± standard deviation		Log ₁₀ removal at HRT ± standard deviation		Log ₁₀ removal at HRT ± standard deviation	
60s	120s	60s	120s	60s	120s	60s	120s
2.21± 0.16	3.14 ± 0.03	1.07± 0.27	1.07± 0.21	0.26± 0.27	0.15± 0.12	0.21± 0.27	0.78± 0.08
1.29± 0.12	1.72± 0.01	0.42± 0.60	0.27± 0.01	0.09± 0.36	0.46± 0.01	0.15± 0.03	0.30± 0.04
1.02± 0.13	1.60± 0.07	0.15± 0.23	0.11± 0.12	0.20± 0.10	0.40± 0.09	0.17± 0.01	0.34± 0.13
1.19± 0.02	1.49± 0.07	0.43± 0.56	0.23± 0.07	0.12± 0.07	0.20± 0.16	0.40± 0.45	0.21± 0.08
1.49± 0.05	2.30± 0.08	0.03± 0.10	0.19± 0.11	0.46± 0.15	0.70± 0.06	0.27± 0.05	0.50± 0.16
1.24± 0.15	1.80± 0.03	-0.43± 0.76	-0.19± 1.09	0.52± 0.01	0.70± 0.09	0.11± 0.32	0.30± 0.33
1.23± 0.01	1.40± 0.08	0.79± 0.65	-1.27± 2.31	0.32± 0.06	0.59± 0.04	-0.11± 0.55	-0.11± 0.65
1.68± 0.10	2.48± 0.08	-	-	-	-	-	-
1.60± 0.12	1.95± 0.03	-	-	-	-	-	-
1.06± 0.08	1.70± 0.15	-	-	-	-	-	-

440

441 3.2 Impact of operating conditions on PUV irradiation

442 Overall, a linear relationship was observed between voltage and inactivation rate for any
 443 given HRT (Figure 3). FRNA bacteriophage (GA) concentration was reduced by 1.3 log₁₀ at
 444 a UV dose of 1.2 J/cm² (1200 mJ/cm²; 120 s HRT) when subjected to 900 V at 1 PPS. A
 445 reduction of 1.0 log₁₀ was achieved at a UV dose of 0.55 J/cm² (550 mJ/cm²; 120 s HRT) at
 446 600 V and 1 PPS; whereas at 300 V and 1 PPS, a maximum virus reduction of 0.4 log₁₀ was
 447 observed at a UV dose of 0.14 J/cm² (140 mJ/cm²; 120 s HRT); thus demonstrating the
 448 impact of HRT on inactivation.

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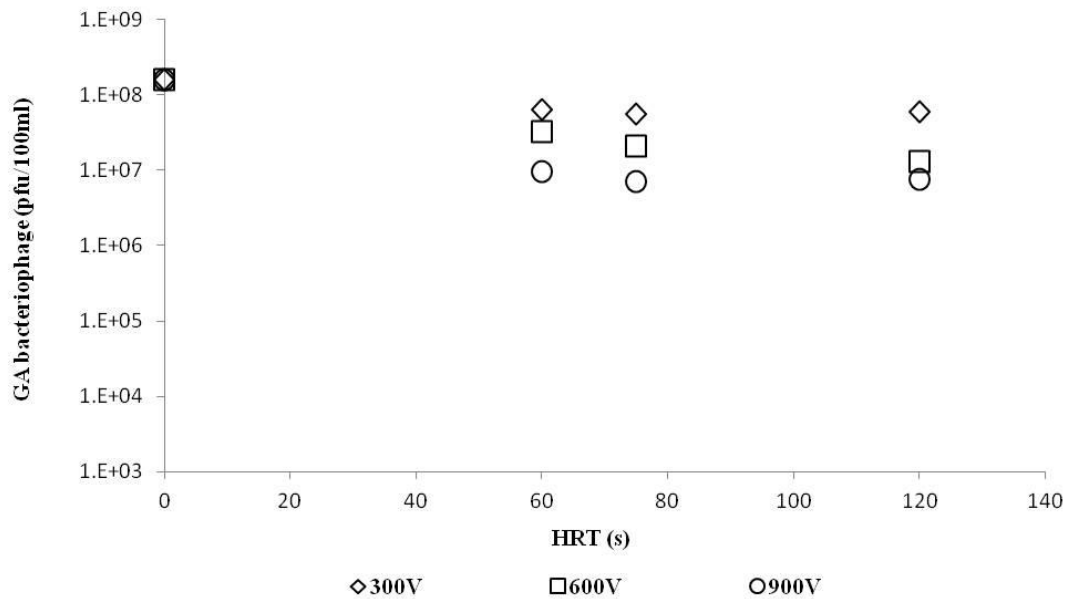


Figure 3. The effect of three specific voltages (300, 600 and 900 V) and three HRTs (60, 75 and 120 s) at 1 PPS on FRNA bacteriophage (GA) reduction.

3.3 Comparison of on-site LP UV and bench-scale PUV systems

Figures 4A, 4B and 4C summarizes the comparative reduction of *E. coli*, total coliforms and FRNA bacteriophage for the LP UV and PUV. A reduction in *E. coli*, total coliforms and FRNA bacteriophage concentrations was observed in response to increasing UV dose. Comparative reduction rates between LP UV and PUV under varying doses are illustrated in Table 4. Previous studies have observed the PUV showing a significantly greater inactivity potential compared to LP UV when using *E. coli* as a bacterial indicator organism (Li *et al.*, 2010). However in this study such a difference was not apparent at similar radiation dosages.

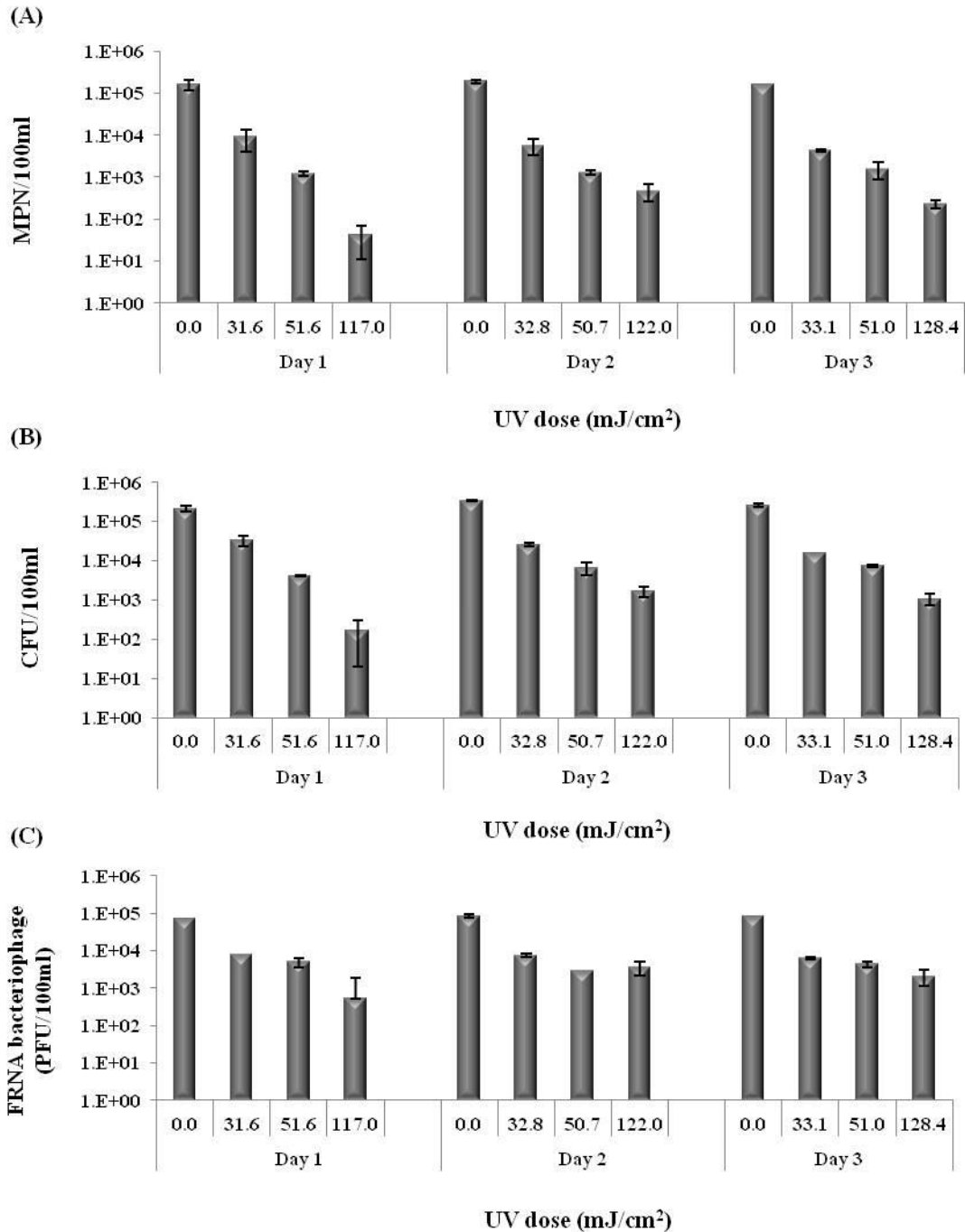


Figure 4. (A) *E. coli* reduction via LP UV over three separate trials (B) Total coliforms reduction via LP UV over three separate trials (C) FRNA bacteriophage reduction via LP UV over three separate trials.

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Table 4. (A) Comparison of the operating conditions for the treatment of secondary treated wastewater employing on – site LP UV system (LP UV) and bench – scale PUV system (PUV).

Day	UV treatment	Flow Rate (m ³ /hr)	HRT (s)	UV Dose - J/cm ² (mJ/cm ²)
1	LP UV	0.228	3.9	0.117 (117)
	LP UV	0.52	1.7	0.05161 (51.61)
	LP UV	0.849	1.1	0.03161 (31.61)
	PUV	0.04	60	3.4478 (3447.8)
2	LP UV	0.22	4.1	0.12199 (121.99)
	LP UV	0.529	1.7	0.05073 (50.73)
	LP UV	0.818	1.1	0.03281 (32.81)
	PUV	0.04	60	3.4478 (3447.8)
3	LP UV	0.22	4.3	0.12841 (128.41)
	LP UV	0.529	1.7	0.05102 (51.02)
	LP UV	0.818	1.1	0.03313 (33.13)
	PUV	0.04	60	3.4478 (3447.8)

485

486 Table 4 (B) provides a comparison for indicative purposes and outlines the removal of *E.*
 487 *coli*, *Bacillus subtilis* (*B. subtilis*) and GA bacteriophage via PUV both in this study and in
 488 recent work by Uslu *et al.* (2014). In contrast to this study where the PUV was operated as a
 489 flow through system, Uslu *et al.* (2014) operated it as a static system. Recent studies
 490 employing PUV as a wastewater disinfection tool have indicated that in addition to pathogen
 491 removal/inactivation it also reduces the organic load of municipal wastewater effluent by
 492 reducing chemical oxygen demand (COD) and total organic carbon (TOC; Uslu *et al.*, 2016).
 493 Furthermore evidence suggests that the treatment with PUV enables the targeting and
 494 removal of pathogenic biofilm forming microbes, such as *Pseudomonas aeruginosa* and

495 *Staphylococcus aureus*, which are often resistant to common disinfection strategies (Garvey
 496 *et al.*, 2015). Additionally, its role in the breakdown and removal of industrial related
 497 pollutants such as azo dyes represent a novel application in the treatment of chemically
 498 contaminated wastewater and the protection of the environmental (Li *et al.*, 2016).

499

500

Table 4. (B) Microorganism reduction via PUV treatment

Uslu <i>et al.</i> (2014)						
PUV operating conditions	Voltage: 3,800 V sample: 8cm Capacitance: N/A System set-up: Static wastewater			Lamp Distance from Discharge time: 360 μ s Medium: Treated municipal		
Microorganism	<i>E. coli</i>			<i>B. subtilis</i>		
Initial concentration	10 ⁸ CFU/mL			10 ⁹ CFU/mL		
SS (mg/L)	4			4		
Exposure time (s)	5	10	15	5	10	15
Broadspectrum Dose - J/cm ² (mJ/cm ²)	3.6 (3600)	7.2 (7200)	10.9 (10900)	3.6 (3600)	7.2 (7200)	10.9 (10900)
Log ₁₀ removal (CFU/mL)	\approx 7 log	\approx 7 log	Complete reduction (undetected)	\approx 4 log	\approx 4 log	\approx 6 log
This study						
PUV operating conditions	Voltage: 900 V sample: 10.75cm Capacitance: 40 μ F System set-up: Flow-through wastewater			Lamp Distance from Discharge time: 28 μ s Medium: Treated municipal		
Microorganism	<i>E. coli</i>			GA bacteriophage		
Initial concentration	10 ⁵ MPN/100mL			10 ⁷ PFU/mL	10 ⁷ PFU/mL	10 ⁶ PFU/mL
SS content (mg/L)	28			20	38	72
Exposure time (s)	60			120	120	120
Broadspectrum Dose - J/cm ² (mJ/cm ²)	18.8 (18800)			37.5 (37500)	37.5 (37500)	37.5 (37500)
Log ₁₀ removal	2 log ₁₀ MPN/100ml			2.48 log ₁₀ PFU/100mL	2.30 log ₁₀ PFU/100mL	1.95 log ₁₀ PFU/100mL

501 **3.4 Impact of wastewater characteristics on PUV efficiency**

502 Table 5 summarises the results of the trials carried out to determine the impact of wastewater
 503 characteristics on FRNA bacteriophage (GA) disinfection via the PUV. There was little
 504 evidence of TOC and TIC concentrations impacting on the overall log₁₀ reduction of FRNA
 505 bacteriophage PFU (GA) decreased (SM 1) with mixed trends observed in each trial. Within
 506 trials 3 and 4 high correlations for each individual trial between SS concentration and FRNA
 507 bacteriophage (GA) PFU log₁₀ reduction was observed. However, a relatively low statistical
 508 correlation (- 0.42) was observed between higher SS concentrations and decreasing log₁₀
 509 reductions of GA bacteriophage across all samples. Thus may indicate that FRNA log₁₀
 510 reductions may be influenced by factors other than the SS concentrations (Figure 5).

511

512 **Table 5.** PUV log₁₀ reductions of infective FRNA bacteriophage (GA) in wastewater at two
 513 HRTs at a range of sample SS, TOC and TIC concentrations (mg/L; Trial 1 not included; 60 s
 514 HRT: UV dose – 3.4 J/cm² (3400 mJ/ cm²) and 120 s HRT: UV dose 6.9 J/cm² (6900 mJ/
 515 cm²); the average initial concentration was 10⁶/100 mL).

516

Trial	Wastewater characteristics			Log ₁₀ reduction	
	SS (mg/L)	TOC (mg/L)	TIC (mg/L)	HRT	
				60 (s)	120 (s)
2	57.5	8	24	2.2 ± 0.2	3.1 ± 0.0
	12.0	14	41	1.3 ± 0.1	1.8 ± 0.0
	18.6	20	38	1.0 ± 0.1	1.6 ± 0.1
	121.2	20	39	1.2 ± 0.0	1.5 ± 0.1
3	38.0	10	33	1.5 ± 0.1	2.3 ± 0.1
	105.0	8	32	1.2 ± 0.2	1.8 ± 0.0
	140.6	7	29	1.2 ± 0.0	1.4 ± 0.1
4	19.5	12	25	1.7 ± 0.1	2.4 ± 0.1
	72.0	16	26	1.6 ± 0.1	1.2 ± 0.0
	89.8	15	28	1.1 ± 0.1	1.7 ± 0.2

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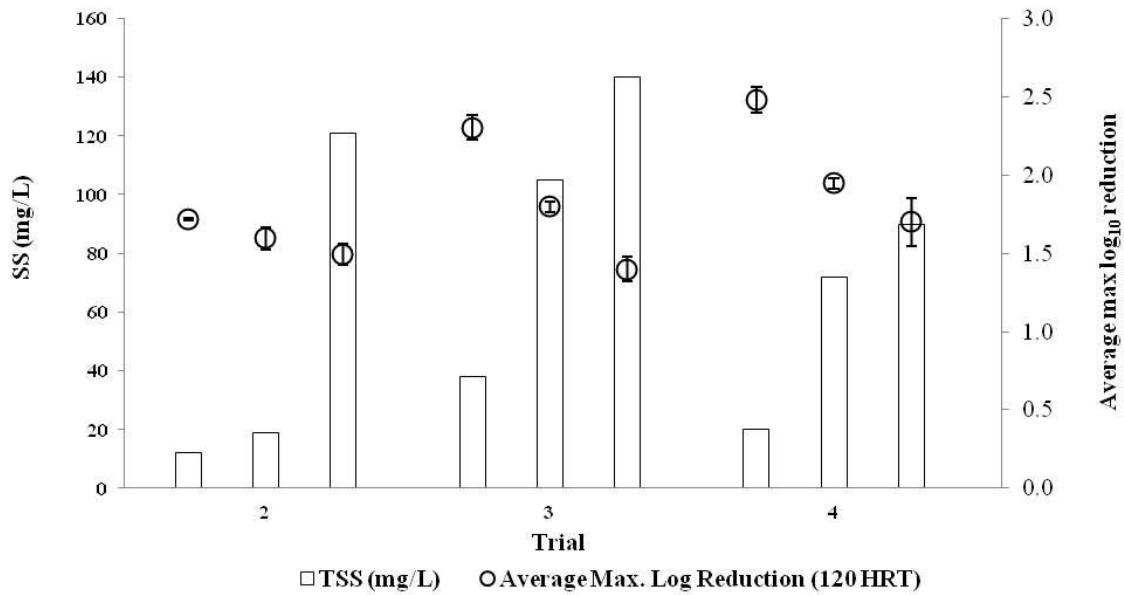


Figure 5. The relationship between SS and maximum log₁₀ reduction (HRT 120 s– UV dose: 6.9 J/cm² (6900 mJ/cm²) of GA bacteriophage via infectivity assay in three separate trials. (The average initial concentration was 10⁶/100 mL).

During the study, the effluent wastewater from WWTPs 1, 2 and 3 was sampled with both filtered and unfiltered samples being subjected to PUV treatment. The SS concentrations of the treated wastewater at WWTPs 1, 2 and 3 were 19.5 mg SS/L, 8.7 mg SS/L and 16.0 mg SS/L, respectively; indicating the possibility of varying efficiency of secondary treatment in the respective WWTP's. Results indicate that the removal of SS within for any given WWTP resulted in improved PUV performance; however appeared to be unrelated to the initial SS (albeit the effluent samples all had relatively low SS concentrations). Following filtration of the secondary effluent obtained from WWTP 1, a 3.9 log₁₀ reduction was recorded. Furthermore, virus inactivation to below the level of detection (< 1 pfu/mL) was achieved at a UV dosage of 3.4 J/cm² (3400 mJ/cm²); HRT of 60 s; Table 6). Increased virus log₁₀ reduction in filtered effluent compared to unfiltered effluent was also observed for WWTPs 2 and 3. However, complete viral removal was not achieved at a UV dosage of 6.9 J/cm² (6900 mJ/cm²) and a maximum HRT (120 s) indicating that alternative environmental parameters were playing a role effecting UV efficacy.

546 **Table 6.** Comparison of maximum log₁₀ reduction (120s HRT) of FRNA bacteriophages
 547 (GA) in filtered and unfiltered post-secondary treatment effluent treated with PUV at three
 548 separate WWTP sampling sites. (UV dose – 3.4 J/cm² (3400 mJ/cm²) and 120 seconds (s)
 549 (UV dose: 6.9 J/cm² (6900 mJ/cm²); the average initial concentration was 10⁶/100 mL)
 550

	Unfiltered Effluent		Filtered Effluent	
	HRT (s)	<u>FRNA bacteriophages (GA)</u>	HRT (s)	<u>FRNA bacteriophages (GA)</u>
		(pfu/100ml)		(pfu/100ml)
WWTP Site 1	0	1.2E+07 ± 6.4E+05	0	2.3E+06 ± 1.8E+05
	60	2.5E+05 ± 4.4E+04	60	< 1 pfu/mL
	120	3.9E+04 ± 4.9E+03	120	< 1 pfu/mL
Maximum Log₁₀ Reduction		2.5 ± 0.1		6.4 ± 0.0
WWTP Site 2	0	1.5E+07 ± 9.7E+05	0	1.5E+07 ± 1.1E+06
	60	2.7E+05 ± 6.7E+04	60	9.5E+04 ± 2.3E+04
	120	6.4E+04 ± 2.0E+04	120	7.0E+03 ± 1.4E+03
Maximum Log₁₀ Reduction		2.4 ± 0.1		3.3 ± 0.1
WWTP Site 3	0	1.1E+06 ± 7.1E+04	0	1.1E+07 ± 4.6E+06
	60	3.7E+04 ± 7.5E+03	60	8.1E+04 ± 3.8E+04
	120	2.4E+04 ± 7.8E+03	120	3.8E+04 ± 3.4E+04
Maximum Log₁₀ Reduction		1.7 ± 0.2		2.5 ± 0.3

551

552 Further analysis was carried out on these samples to determine if alternative contributing
 553 factors within the effluent which may have interfered with PUV efficiency. TOC and TIC
 554 were measured against FRNA bacteriophage (GA) log₁₀ reduction (SM 1). A low statistical
 555 correlation was found between both variables however a slight trend was apparent between
 556 high TOC and TIC concentrations and decreasing virus log₁₀ reductions (SM 1). In addition
 557 to this, sporadic checks for iron and manganese were carried out as literature indicated this
 558 play a role in inhibiting UV performance. No significant impact was recorded indicating that
 559 levels were insufficient enough to induce an effect (data not shown), which is in keeping with
 560 the characteristic municipal nature of the effluent.

561

562 The effectiveness of UV disinfection in wastewater treatment relies heavily on the
 563 performance of upstream processes. While primary and secondary treatment of wastewater
 564 has demonstrated somewhat efficient removal of pathogens it is widely accepted that a
 565 suitable efficient robust tertiary treatment can increase these removal/inactivation rates
 566 greatly (Koivunen *et al.*, 2003). High concentrations of suspended solids in secondary treated
 567 wastewater, which can result from poor upstream process control or various stresses on

568 upstream processes, have a direct effect on the efficacy of UV disinfection systems. For
569 example relatively high suspended solids concentrations can shield microbes from UV rays
570 and result in bio-fouling of submerged UV lamp systems. Therefore UV is often used in
571 conjunction with an alternative method of disinfection, such as pre-rapid sand filtration
572 (Rajala *et al.*, 2003).

573

574 This study also highlights that SS can indeed play a key role in impacting PUV performance;
575 however the magnitude of the impact may be WWTP specific and thus require site specific
576 pre-treatment amendments (Table 6). It reaffirms the strong interaction between viral loads
577 and suspended solids indicating the need for continuous monitoring of upstream applications
578 to ensure no compact solids filter through to the tertiary stage, protecting viral particles and
579 thus rendering the disinfection process inefficient (Gehr *et al.*, 2003; da Silva *et al.*, 2007;
580 Flannery *et al.*, 2012). It should be noted that further study into the disposal of wastewater
581 sludge may need to consider the presence of such viruses.

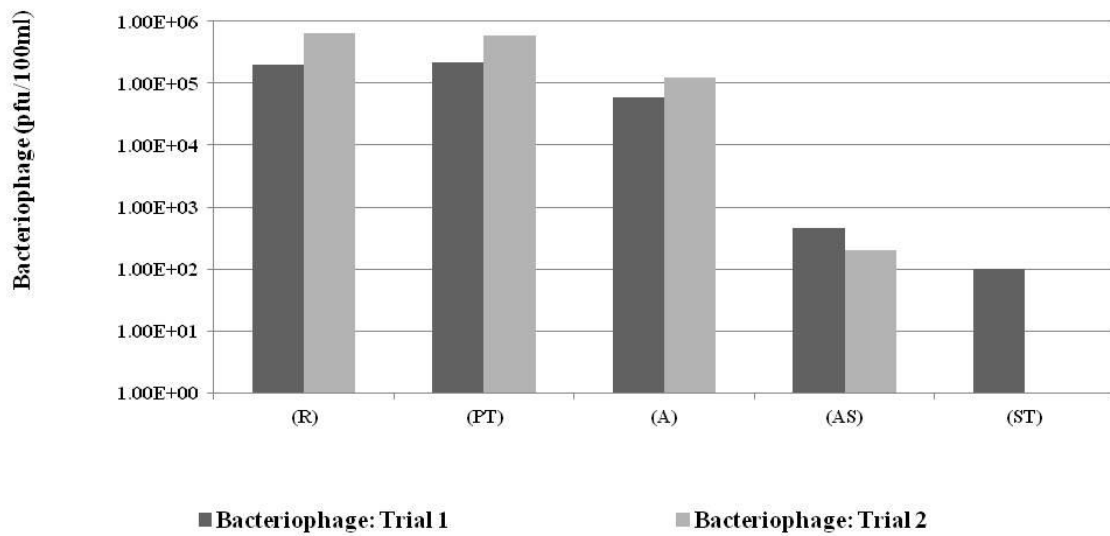
582

583 **3.4 Fate and persistence of NoV through a WWTP using surrogate FRNA** 584 **bacteriophage**

585 The fate of FRNA bacteriophage was monitored through WWTP 1 and the results are
586 summarized in Figure 6. Following the settling of the activated sludge sample (A), a greater
587 than 2 log₁₀ reduction of FRNA bacteriophage was observed in the clarified wastewater (AS)
588 after settling.

589

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591

592 **Figure 6.** Concentration of infectious FRNA bacteriophage (pfu/100mL) at selected sampling
 593 locations in WWTP1 (R- Raw Influent; PT – Primary Treatment; A – Activated Sludge; AS –
 594 Activated Sludge ‘clarified wastewater post sludge settled’; ST – Secondary treatment; n= 2).
 595 SS was also recorded (Trial 1: R = 180 mg/L; PT = 120 mg/L; A = 8427 mg/L; AS = 0; ST =
 596 3) (Trial 2: R = 287 mg/L; PT = 150 mg/ml; A = 7767 mg/L; AS = 57; ST = 47; (The average
 597 initial concentration was $10^5/100$ mL).
 598

599 Wastewater systems that treat both municipal wastewater and storm water are at high risk as
 600 large rainfall occurrences can overwhelm the wastewater treatment system resulting in
 601 inefficient treatment and solid release. These rainfall occurrences can be prevalent in the
 602 winter months when the prevalence of NoV is traditionally high according to published
 603 epidemiological studies (Galmore *et al.*, 2007). Nordgren *et al.* (2009) found that using
 604 RTqPCR, NoV GI and GII exhibited seasonal variance with the highest concentrations
 605 recorded in the winter months. The study monitored its prevalence through a WWTP over
 606 one year targeting 8 particular treatment points during the process. They noted a 0.7 log
 607 reduction in NoV during primary treatment in an activated sludge treatment plant. Similarly,
 608 Flannery *et al.* (2012) noted a comparable seasonal trend indicating the concentrations of GI,
 609 GII were higher in winter months, interestingly no seasonal variation were seen with respect
 610 to FRNA bacteriophage (GA) concentration. Moreover, they noted that NoV GI and GII log
 611 removal was 0.13 and 0.14 respectively following primary treatment. Comparison of NoV
 612 and FRNA bacteriophage (GA) reduction during secondary treatment is difficult as often
 613 varying secondary treatment methodologies are employed.
 614

615 **4.0 Conclusion**

616 It is clear that the use of viral inactivation technologies is seen as an increasingly necessary
617 part of the wastewater treatment processes. Key drivers for their implementation include
618 legislation, public health, tourism and commercial demands for clean water (or reuse of
619 wastewater). While there have been on-going technological and research developments in this
620 sector it is not possible to recommend a single best solution. Thus on-site considerations are
621 the key element in choosing a disinfection system for any given application. While no
622 comparative link could be made between NoV GI, NoV GII and the surrogate FRNA
623 bacteriophage (GA) in this study, several alternative studies have indicated a link using
624 alternative surrogates which warrant further investigation under the conditions outlined
625 above. Settling processes prior to treatment determines the fate of NoV and FRNA
626 bacteriophage (GA) in a WWTP as greater than 3 log₁₀ reduction of FRNA bacteriophage
627 was observed in the clarified wastewater (AS) after settling occurred. As the SS concentration
628 in the effluent sample increased, the maximum log₁₀ reduction of FRNA bacteriophage (GA)
629 PFU decreased for any given trial. It is worth noting that this trend varied and appeared to be
630 site specific, therefore this study was unable to deduce SS allowable limits for efficient UV
631 treatment.

632

633 This finding warrants further investigations as pre-treatment could greatly decrease the risk of
634 viral-loaded effluent which may pass though tertiary treatment shielded by SS. Results
635 indicate that the adsorption of viral particles to solids in wastewater occurs. As such, a twin
636 tertiary treatment may be the best method of choice. Particularly in areas prone to turbid
637 secondary treated wastewater where a barrier process such as tangential flow filtration system
638 (TFF), filters the particulate matter and the flow through is treated with UV. Results highlight
639 the importance of optimal performance of upstream primary and secondary WWTP processes
640 highlighting how vital continuous monitoring is to ensure the SS are kept low. Results
641 indicate that whilst SS may indeed affect LP UV and PUV treatment efficacy,
642 additional/alternate environmental parameters may indeed play an unknown role.

643

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